

Abstract

Headwind or tailwind?

Defossilization in the chemicals industry

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Summary

1 2 The chemicals industry is an industry built on carbon – approximately 450 mn tons in feedstock, 330 mn tons in energy consumption, and 100 mn tons in unavoidable process emission¹

From material aspect, recycled, bio-based, waste-based, and CO2-based gain significant trajectory; however, the majority (>75%) will be served by fossil sources by 2030

From energy perspective, optimized reaction engineering, efficiency improvement, waste heat recovery, and sustainable alternative energy sources will make major contribution

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Unavoidable emission through production processes and energy consumption should be captured for utilization or permanent storage



Despite clear guiding principles, defossilization of the chemicals industry is facing significant challenges, especially in scalability and costs



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With proper (regulatory) incentives and maturing technology, certain solutions show attractive economic viability

Cross-industry collaboration and openness to technology are required to build up a sustainable and financially viable new ecosystem at scale

1) 2022 data

Carbon feedstock demand of the chemical industry is to reach approximately 590 mt by 2030; only minor part will be covered by sustainable carbon sources

Carbon demand of the global chemicals industry, _____ 2022 [mt carbon]



Embedded carbon in feedstock
Carbon from energy demand
Indirect carbon from processes



1 Recycled carbon

- Recycling with highest technological readiness
- Significant shortcomings in global waste supply and quality as key limiting factors

Biobased carbon

- Direct competition to food and feed in 1st generation processes
- 2nd generation for commodities as bioethanol commercialized
- Moderate tech. readiness and high cost of 3rd generation (algae) processes
- Drop-in solution with lower capex requirement

🦉 </u> 3 Utilized carbon

- CCU technology least advanced and high capex requirement
- For most products 10-20 years required to become large-scale commercialization
- While direct air capture being least economic, many high concentration CO₂ emitters exist

Under favorable regulation conditions, CCS can be economically viable, e.g., within the IRA, ~30% of emission can be abated under attractive financial viability

2030 marginal abatement cost curve for Chemicals & Refining industry, with IRA in the US [USD/t CO₂]



1) Heat electrification analysis include IRA 48E incentive assuming the projects meet the prevailing wage and apprenticeship requirements, and half of projects meets qualify for the domestic content adder. ITC incentives are not considered in this analysis due to unclear economic impact (e.g., state and local impact) and local impact (e.g., state and local policies. Asset and geography specific considered in this analysis due to unclear economic impact (e.g., state and local impact) and local impact (e.g., state and local policies. Asset and geography specific considered in this analysis due to unclear economic impact (e.g., state and local impact) and local impact (e.g., state and local policies. Asset and geography specific considered in this analysis due to unclear economic impact (e.g., state and local policies. Asset and geography specific considered in this analysis due to unclear economic impact (e.g., state and local impact) and local impact (e.g., state and local policies. Asset and geography specific constant.

2) Electrification of compressor results in significant efficiency improvements over steam turbines (95% versus 35% efficiency)

3) Renewable cost assumes Class 5 anshore wind production from NREL Annual technology Baseline for 2030 and excludes the costs associated with transmission and delivery of electricity. IRA-inclusive scenarios include investment tax credit of 35%, 30% from a base construction that meets the prevailing wage and apprenticeship requirements and an additional 5% due to an assumption that half of projects will claim the 10% domestic content addres. No addres included for law-index for address and additional 5% due to an assumption that half of projects will claim the 10% domestic content addres. No addres included for law-index for address and additional 5% due to an assumption that half of projects will claim the 10% domestic content addres. No address included for law-index for address and additional 5% due to an assumption that half of projects will claim the 10% domestic content address.

4) Heat generation technology assumes the costs associated with charging and TES as an orchetypical setup, however, asset specific considerations could significantly impact the choice of heat generation technology

Ethylene process assumptions used to model propylene and BTX processes (e.g., propane and naphth)

Displayed CCS cost estimates based on EFI foundation capture costs with transport (GCCSI, 2019) and storage (BNEF, 2022) costs -\$10-40 tonne (representing the lower and upper bounds of the displayed range) except where noted. All in 2022 dollars. All CCS figures represent retrofits, not new-build facilities. The inflation variance on each cost estimate represents the range of cost increases on a generic chemical processing plant upper bounds of the displayed range) except where noted. All in 2022 dollars. All CCS figures represent retrofits, not new-build facilities. The inflation variance on each cost estimate represents the range of cost increases on a generic chemical processing plant upper bounds of the displayed range) except where noted. All in 2022 dollars. All CCS figures represent retrofits, not new-build facilities. The inflation variance on each cost estimate represents the range of cost increases on a generic chemical processing plant upper bounds of the displayed range) except where noted. All in 2022 dollars. All CCS figures represent retrofits, not new-build facilities. The inflation variance on each cost estimate represents the range of cost increases on a generic chemical processing plant upper bounds of the displayed range) except where noted. All in 2022 dollars. All CCS figures represent retrofits, not new-build facilities. The inflation variance on each cost estimate represents the range of cost increases on a generic chemical processing plant upper bounds of the displayed range) except where noted.

The range of 2030 electrolytic hydrogen costs for refining is estimated at \$22-1.22 / kg H2. All hydrogen for ammonia is estimated at \$28-1.28 / kg H2. All hydrogen cost assumptions for this modeled scenario are based on DOE's Clean Hydrogen Lift-off, which relief on the 2022 McKinsey Hydrogen Model. The impact of the 45V tax credit is modeled as \$1.80 / kg H2 reduction in OpEx cost, based on assumptions for this modeled scenario are based on DOE's Clean Hydrogen for ammonia is estimated at \$2.8-1.28 / kg H2. All hydrogen cost assumptions for this modeled scenario are based on DOE's Clean Hydrogen Lift-off, which relief on the 2022 McKinsey Hydrogen Model. The impact of the 45V tax credit is modeled as \$1.80 / kg H2 reduction in OpEx cost, based on assumptions of 10% MACC, 10 years of tax credit, and a 20-year project lifetime. It is important to note that the assumptions underlying this analysis are uncertain, and the Clean Hydrogen Lift-off report is continually being updated. DoE electrolyser cost estimates have already increased since the value published in this report due to variable such as supply chain constraints and inflation. Additionally, the impacts of tax incentives on cost will be subject to available such as underlying the impact so that as a supply chain constraints and inflation. Additionally, the impacts of tax incentives on cost will be subject to available such as the value published in this report due to variable such as the value published in this report is continually being updated. DoE electrolyser cost estimates have already increased since the value published in this report due to variable such as supply chain constraints and inflation. Additionally, the impacts of tax incentives on cost will be subject to variable such as the value published in this report due to variable such as the value published in t

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9) Split of emission streams assumed to be -60% concentrated and -40% dilute in SMR unit. Portion of SMR concentrated streams assumed to be smaller for ammonia due to captive usage of concentrated CO2 streams for urea producti

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NGP: next generation geothermal power; SMR: steam methane reforming; LDES: long distance energy storage; TES: thermal energy storage; FCC: fluid catalytic cracking

Source: GREET 2022, NREL, DOE Hydrogen Liftoff Report, EFI CCS report - "Turning CCS projects in heavy industry & power into blue chip financial investments", Inflation Reduction Act, LDES Council, Expert interviews, Danish Energy Agency, OHG Protocol, White House net-zero targets, McKinsey Global Energy Perspective, EFI Foundation, "Turning CCS Projects in heavy industry & power into blue chip financial investments", Roland Berger 4



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